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(54) Title: HYDROFORMYLATION PROCESS

(57) Abstract: Embodiments of the present invention are directed to processes to improve rhodium accountability in continuous liquid recycle hydroformylation processes. In some embodiments, a process comprises contacting in a reaction zone reactants comprising mixed C8 olefins or mixed C9 olefins, hydrogen, and carbon monoxide in the presence of a catalyst comprising rhodium and an organomonophosphite ligand to form a reaction fluid, wherein the reaction fluid is introduced to a strip gas vaporizer to produce a product stream and a vaporizer tails stream, and wherein the vaporizer tails stream comprises at least 1.2 percent by weight C8 internal olefins or at least 1.3 percent by weight C9 internal olefins.



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HYDROFORMYLATION PROCESS

FIELD

The present invention relates to processes to improve rhodium accountability in a
5 continuous liquid recycle hydroformylation process.

BACKGROUND

It is well known that aldehydes can be produced by reacting olefins with carbon
monoxide and hydrogen in the presence of a metal-organophosphorus ligand complex
catalyst. Such processes can involve continuous hydroformylation and recycling of a
10 catalyst solution containing a metal-organophosphorus ligand complex catalyst wherein the
metal is selected from Groups 8, 9, or 10. Rhodium is a common Group 9 metal used in the
metal-organophosphorus ligand complex catalyst for hydroformylation. Examples of such a
process are disclosed in U.S. Patent Nos. 4,148,830, US 4,717,775, and US 4,769,498. The
resulting aldehydes can be used to produce a host of products including alcohols, amines,
15 and acids.

Hydroformylation catalysts comprising rhodium and bulky organomonophosphite
ligands are capable of very high reaction rates. *See, e.g.*, "Rhodium Catalyzed
Hydroformylation," van Leeuwen, Claver, Kluwer Academic Pub. (2000). Such catalysts
have industrial utility as they can be used to increase production rates, or to efficiently
20 hydroformylate internal and/or branched internal olefins which react more slowly than
linear alpha olefins.

Under some conditions, rhodium-bulky organomonophosphite catalysts have been
known to suffer an irretrievable loss of rhodium in liquid recycle hydroformylation
processes. *See, e.g.*, U.S. Patent No. 4,774,361. Although the exact cause of rhodium loss
25 is unclear, it has been hypothesized that the rhodium loss is exacerbated by the product
separation step, which is commonly achieved through vaporization and condensation of the
product overhead, leaving a residual stream that includes higher boiling by-products and the
non-volatile catalyst (vaporizer tails) which is then recycled back to the reaction zone.
Vaporization of the products derived from higher olefins (e.g., C8 or higher) requires higher
30 temperatures which are also known to exacerbate rhodium loss. A continuous loss of
rhodium can increase catalyst costs dramatically, as rhodium is prohibitively expensive.

There remains a need for continuous liquid recycle hydroformylation processes that improve rhodium accountability, particularly when hydroformylating C8 or higher olefins using highly active rhodium-organomonophosphite catalysts.

SUMMARY

5 The present invention relates to processes for hydroformylating C8 or C9 olefins using continuous liquid recycle that improve rhodium accountability. It has been surprisingly found that by maintaining a concentration of at least 1.2 percent by weight of C8 internal olefins in a vaporizer tails stream from a strip gas vaporizer, the rhodium accountability will improve. That is, the amount of rhodium loss in the process will be
10 reduced.

 In one aspect, a process to improve rhodium accountability in a continuous liquid recycle hydroformylation process comprises contacting in a reaction zone reactants comprising mixed C8 olefins and/or mixed C9 olefins, hydrogen, and carbon monoxide in the presence of a catalyst comprising rhodium and an organomonophosphite ligand to form
15 a reaction fluid, wherein the reaction fluid is introduced to a strip gas vaporizer to produce a product stream and a vaporizer tails stream, and wherein the vaporizer tails stream comprises at least 1.2 percent by weight C8 internal olefins or at least 1.3 percent by weight C9 internal olefins.

 In one aspect, a process to improve rhodium accountability in a continuous liquid
20 recycle hydroformylation process comprises contacting in a reaction zone reactants comprising mixed C8 olefins, hydrogen, and carbon monoxide in the presence of a catalyst comprising rhodium and an organomonophosphite ligand to form a reaction fluid, wherein the reaction fluid is introduced to a strip gas vaporizer to produce a product stream and a vaporizer tails stream, and wherein the vaporizer tails stream comprises at least 1.2 percent
25 by weight C8 internal olefins.

 In another aspect, a process to improve rhodium accountability in a continuous liquid recycle hydroformylation process comprises contacting in a reaction zone reactants comprising mixed C9 olefins, hydrogen, and carbon monoxide in the presence of a catalyst comprising rhodium and an organomonophosphite ligand to form a reaction fluid, wherein
30 the reaction fluid is introduced to a strip gas vaporizer to produce a product stream and a vaporizer tails stream, and wherein the vaporizer tails stream comprises at least 1.3 percent by weight C9 internal olefins.

These and other embodiments are discussed in more detail in the Detailed Description below.

BRIEF DESCRIPTION OF THE FIGURE

Figure 1 illustrates the relationship between the average C8 internal olefin concentration in a fluid within the strip gas vaporizer and the corresponding concentration of C8 internal olefins in the vaporizer tails stream for Examples of Table 6.

DETAILED DESCRIPTION

All references to the Periodic Table of the Elements and the various groups therein are to the version published in the CRC Handbook of Chemistry and Physics, 72nd Ed. (1991-1992) CRC Press, at page I-11.

Unless stated to the contrary, or implicit from the context, all parts and percentages are based on weight and all test methods are current as of the filing date of this application. For purposes of United States patent practice, the contents of any referenced patent, patent application or publication are incorporated by reference in their entirety (or its equivalent U.S. version is so incorporated by reference).

As used herein, “a,” “an,” “the,” “at least one,” and “one or more” are used interchangeably. The terms “comprises,” “includes,” and variations thereof do not have a limiting meaning where these terms appear in the description and claims.

Also herein, the recitations of numerical ranges by endpoints include all numbers subsumed in that range (e.g., 1 to 5 includes 1, 1.5, 2, 2.75, 3, 3.80, 4, 5, etc.). For the purposes of the invention, it is to be understood, consistent with what one of ordinary skill in the art would understand, that a numerical range is intended to include and support all possible subranges that are included in that range. For example, the range from 1 to 100 is intended to convey from 1.01 to 100, from 1 to 99.99, from 1.01 to 99.99, from 40 to 60, from 1 to 55, etc.

As used herein, the term “ppmw” means parts per million by weight.

For purposes of this invention, the term “hydrocarbon” is contemplated to include all permissible compounds having at least one hydrogen and one carbon atom. Such permissible compounds may also have one or more heteroatoms. In a broad aspect, the permissible hydrocarbons include acyclic (with or without heteroatoms) and cyclic, branched and unbranched, carbocyclic and heterocyclic, aromatic and nonaromatic organic compounds that can be substituted or unsubstituted.

As used herein, the term “substituted” is contemplated to include all permissible substituents of organic compounds unless otherwise indicated. In a broad aspect, the permissible substituents include acyclic and cyclic, branched and unbranched, carbocyclic and heterocyclic, aromatic and nonaromatic substituents of organic compounds. Illustrative substituents include, for example, alkyl, alkyloxy, aryl, aryloxy, hydroxyalkyl, aminoalkyl, in which the number of carbons can range from 1 to 20 or more, preferably from 1 to 12, as well as hydroxy, halo, and amino. The permissible substituents can be one or more and the same or different for appropriate organic compounds. This invention is not intended to be limited in any manner by the permissible substituents of organic compounds.

As used herein, the term “hydroformylation” is contemplated to include, but is not limited to, all hydroformylation processes that involve converting one or more substituted or unsubstituted olefinic compounds or a reaction mixture comprising one or more substituted or unsubstituted olefinic compounds to one or more substituted or unsubstituted aldehydes or a reaction mixture comprising one or more substituted or unsubstituted aldehydes. The aldehydes may be asymmetric or non-asymmetric.

The terms “catalyst fluid”, “process fluid”, “reaction fluid,” “reaction medium” and “catalyst solution” are used interchangeably herein, and may include, but are not limited to, a mixture comprising: (a) a metal-organomonophosphite ligand complex catalyst, (b) free organomonophosphite ligand, (c) aldehyde product formed in the reaction, (d) unreacted reactants, (e) a solvent for said metal-organomonophosphite ligand complex catalyst and said free organomonophosphite ligand, and, optionally, (f) one or more compounds resulting from degradation of the organomonophosphite ligand; such ligand degradation products may be dissolved and/or suspended. The reaction fluid can encompass, but is not limited to, (a) a fluid in a reaction zone, (b) a fluid stream on its way to a separation zone, (c) a fluid in a separation zone, (d) a recycle stream, (e) a fluid withdrawn from a reaction zone or separation zone, (f) a withdrawn fluid being treated to remove ligand degradation products or other impurities, (g) a treated or untreated fluid returned to a reaction zone or separation zone, (h) a fluid in an external cooler, and (i) ligand decomposition products and components derived from them, such as oxides, sulfides, salts, oligomers, and the like.

“Organomonophosphite ligands” are trivalent phosphorous ligands that contain three P–O bonds.

The term “free ligand” means ligand that is not coordinated to a transition metal.

For the purposes of this invention, the terms “heavy byproducts” and “heavies” are used interchangeably and refer to liquid byproducts that have a normal boiling point that is at least 25 °C above the normal boiling point of the desired product of the hydroformylation process. Such materials are known to form inherently in hydroformylation processes under normal operation through one or more side reactions, including for example, by aldol condensation.

For the purpose of this invention, the term “dimer” in reference to heavies refers to heavy byproducts derived from two molecules of aldehyde. Likewise the term “trimer” refers to heavy byproducts derived from three molecules of aldehyde (e.g. C9 aldehyde trimer).

For the purposes of this invention, the terms “reaction zone” and “reactor” are used interchangeably and refer to a region of the process containing reaction fluid and wherein both olefins and syngas (synthesis gas) are added at elevated temperatures.

For the purposes of this invention, the terms “separation zone” and “vaporizer” are used interchangeably and refer to a region where the reaction fluid is heated (i.e. the temperature is higher than the reaction zone temperature) causing an increase in the vapor pressure of the product aldehyde. The resulting gaseous phase is then passed through a condenser to allow collection of the product as a liquid; the non-volatile concentrated effluent (tails, or vaporizer tails) containing the homogeneous catalyst is then returned to one or more of the reactors. The separation zone may optionally be operated at reduced pressure.

For the purposes of this invention, the term “strip gas vaporizer” refers to a vaporizer featuring a flowing gas that aids in product removal. Details of an exemplary strip gas vaporizer may be found in U.S. Patent No. 8,404,903.

For the purposes of this invention, the term “CO strip gas vaporizer” refers to an embodiment of a strip gas vaporizer wherein the partial pressure of carbon monoxide in the strip gas is ≥ 16 psi [≥ 0.110 MPa]. Details of an exemplary CO strip gas vaporizer may be found in U.S. Patent No. 10,023,516.

For the purposes of this invention, the term “strip gas” refers to the flowing gas employed in a strip gas vaporizer. The strip gas is comprised of CO, and optionally hydrogen, and inert gases (e.g., methane, argon, and nitrogen) and may be added directly to the vaporizer on a continuous basis, as well as small amounts of CO, hydrogen, aldehydes, olefins and alkanes which move from the reaction fluid into the vapor phase during

operation. The aldehyde-laden gaseous effluent from the strip gas vaporizer is passed through a condenser (“strip gas condenser”) to generate a crude liquid product stream, and a stream of uncondensed gases. At least a portion of the uncondensed gases are then recycled to the vaporizer (“recycle gas”) using a compressor or blower. Strip gas thus refers to the gaseous stream flowing through the strip gas vaporizer comprising both fresh gases which are continually introduced to the process, and recycle gas.

For the purposes of this invention, the terms “feed to tails” and “feed to tails ratio” are used interchangeably and refer to the mass of reaction fluid entering the separation zone (e.g., strip gas vaporizer) relative to the mass of vaporizer tails leaving the bottom of the separation zone (e.g., strip gas vaporizer) and returning to the hydroformylation reactors. “Feed to tails” is an indicator of the rate at which volatiles, such as aldehyde product, are removed from the reaction fluid. For example, a “feed to tails ratio” of 2, means that the weight of reaction fluid entering the separation zone (e.g., strip gas vaporizer) is two times greater than the weight of the concentrated effluent returned to the hydroformylation reactors.

For the purposes of this invention, the terms “liquid-recycle”, “liquid-recycle hydroformylation”, and “liquid-recycle process” are used interchangeably and are contemplated to comprise a hydroformylation process wherein the process fluid is introduced to a separation zone to produce a tails stream comprising the catalyst which is returned to the reaction zone. Examples of such processes are given in U.S. Patent Nos. 4,148,830 and 4,186,773.

For the purposes of this invention, the terms “mixed C8 olefins” and “mixed octenes” are used interchangeably and refer to the primary olefin feed comprised of singly unsaturated compounds containing eight carbon atoms and hydrogen. This includes 1-octene, C8 internal olefins and branched terminal olefins such as 2-methyl-1-heptene, 3-methyl-1-heptene, 2-ethyl-1-hexene and the like.

For the purposes of this invention, the term “C8 internal olefins” refers to all isomers of singly unsaturated compounds comprised of eight carbon atoms wherein the double bond is not in the terminal position. Examples of C8 internal olefins include, cis-2-octene, trans-2-octene, cis-3-octene, trans-3-octene, cis-4-octene, trans-4-octene, 3-methyl-2-heptene, 3-methyl-3-heptene, 5-methyl-2-heptene, 5-methyl-3-heptene, 3,4-dimethyl-2-hexene, 3,4-dimethyl-3-hexene, 2,3-dimethyl-3-hexene and the like.

For the purposes of this invention, the terms “mixed C9 olefins” and “mixed nonenes” are used interchangeably and refer to the primary olefin feed comprised of singly unsaturated compounds containing nine carbon atoms and hydrogen. This includes 1-nonene, C9 internal olefins and branched terminal olefins such as 2,3-dimethyl-1-heptene, 4,6-dimethyl-1-heptene, 4,6-dimethyl-2-heptene, 4,6-dimethyl-3-heptene, 2,4-dimethyl-2-heptene, 2,6-dimethyl-1-heptene, 2,6-dimethyl-2-heptene, 2,4,5-trimethyl-1-hexene, 2,4,5-trimethyl-2-hexene, and the like.

For the purposes of this invention, the terms “C9 internal olefins” refers to all isomers of singly unsaturated compounds comprised of nine carbon atoms wherein the double bond is not in the terminal position. Examples of C9 internal olefins include, 2,4-dimethyl-2-heptene, 2,6-dimethyl-2-heptene, 2,4,5-trimethyl-2-hexene, 4,6-dimethyl-2-heptene, 4,6-dimethyl-3-heptene and the like.

For the purposes of this invention, the term “recycled olefin(s)” refers to mixed C8 olefins (or mixed C9 olefins in a C9 process) which have passed at least once through the reaction zone without being hydroformylated, and are then separated from the crude aldehyde product, for example, by distillation. The terms “recycled olefin(s)” and “recycled C8 olefin(s)” (and “recycled C9 olefin(s)” when discussing a C9 process) are used interchangeably herein. At least a portion of the olefin thus recovered is then returned to the reaction zone. Recycled olefin may also be returned to other parts of the process as desired. Recycled C8 olefins are comprised largely of dimethyl hexenes which hydroformylate more slowly than linear octenes or methyl heptenes, thus single pass conversion may decline as the concentration of recycled olefin increases.

Hydrogen and carbon monoxide are required for the process. These may be obtained from any suitable source, including petroleum cracking and refinery operations. Syngas mixtures are preferred as a source of hydrogen and CO.

Syngas (from *synthesis gas*) is the name given to a gas mixture that contains varying amounts of CO and H₂. Production methods are well known and include, for example: (1) steam reforming and partial oxidation of natural gas or liquid hydrocarbons, and (2) the gasification of coal and/or biomass. Hydrogen and CO typically are the main components of syngas, but syngas may contain carbon dioxide and inert gases such as CH₄, N₂ and Ar. The molar ratio of H₂ to CO varies greatly but generally ranges from 1:100 to 100:1 and preferably between 1:10 and 10:1. Syngas is commercially available and is often used as a fuel source or as an intermediate for the production of other chemicals. The most preferred

H₂:CO molar ratio for chemical production is between 3:1 and 1:3 and usually is targeted to be between about 1:2 and 2:1 for most hydroformylation applications.

The olefin starting materials that may be employed in the hydroformylation process of this invention are mixed C8 olefins as defined herein. For example, the mixed C8 olefins include mixtures such as may be obtained via dimerization of mixed butenes comprising 1-butene, cis and trans-2-butene and optionally isobutene. In one embodiment, a stream comprising mixed octenes derived from the dimerization of Raffinate II is employed; such mixtures may be produced, for example by the Dimersol process from Axens (Institut Français du Pétrole, Review, Vol. 37, N° 5, September-October 1982, p 639) or the Octol process from Hüls AG (Hydrocarbon Processing, February 1992, p 45-46). It is understood that the olefin mixtures employed in the process of the invention may also comprise some amount of linear alpha olefins.

In some embodiments, the olefin starting materials are mixed C9 olefins as defined herein. Such mixtures may be available from a variety of sources and may be produced, for example by the process described in Johan A. Martens, Wim H. Verrelst, Georges M. Mathys, Stephen H. Brown, Pierre A. Jacobs "Tailored Catalytic Propene Trimerization over Acidic Zeolites with Tubular Pores", *Angewandte Chemie International Edition* 2005, Volume 44, Issue 35, pages 5687-5690.

It should be understood that embodiments of the present invention are designed for use in processes where the olefin starting materials are either mixed C8 olefins or mixed C9 olefins. However, it should be also understood that in processes designed for the hydroformylation of mixed C8 olefins, a small amount of mixed C9 olefins may also be present in the olefin starting materials. Likewise, it should be also understood that in processes designed for the hydroformylation of mixed C9 olefins, a small amount of mixed C8 olefins may also be present in the olefin starting materials.

A solvent advantageously is employed in the hydroformylation process. Any suitable solvent that does not unduly interfere with the hydroformylation process can be used. The organic solvent may also contain dissolved water up to the saturation limit. In rhodium catalyzed hydroformylation, it may be preferred to employ, as a primary solvent, aldehyde compounds corresponding to the aldehyde products desired to be produced and/or higher boiling aldehyde liquid condensation by-products, for example, as might be produced *in situ* during the hydroformylation process, as described for example in U.S. Patent Nos. 4,148,830 and 4,247,486. Indeed, while one may employ, if desired, any suitable solvent at

the start-up of a continuous process, the primary solvent will normally eventually comprise both aldehyde products and higher boiling aldehyde liquid condensation by-products (“heavies”), due to the nature of the continuous process. The amount of solvent is not especially critical and need only be sufficient to provide the reaction medium with the
5 desired amount of transition metal concentration. Typically, the amount of solvent ranges from about 5 percent to about 95 percent by weight, based on the total weight of the reaction fluid. Mixtures of two or more solvents may also be employed.

The catalyst useful in the hydroformylation process comprises a rhodium-organomonophosphite ligand complex. In general, such catalysts may be preformed or
10 formed in situ and consist essentially of rhodium in complex combination with an organomonophosphite ligand, such as those disclosed for example in U.S. Patent No. 4,567,306 and those discussed below, carbon monoxide and hydrogen.

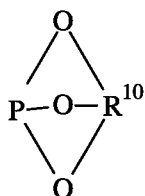
In addition to the organomonophosphite ligand complexed to the metal, additional, or “free” ligand is employed. Mixtures of organomonophosphite ligands may be employed
15 if desired. This invention is not intended to be limited in any manner by the permissible organomonophosphite ligands or mixtures thereof. It is to be noted that the successful practice of this invention does not depend and is not predicated on the exact structure of the metal-organomonophosphite ligand complex species, which may be present in their mononuclear, dinuclear and/or higher nuclearity forms. Indeed, the exact structure is not
20 known. While not intending to be bound to any theory or mechanistic discourse, it appears that the catalytic species may in its simplest form consist essentially of the metal in complex combination with the organomonophosphite ligand and carbon monoxide and/or hydrogen.

The term “complex” as used herein means a coordination compound formed by the union of one or more electronically rich molecules or atoms capable of independent
25 existence with one or more electronically poor molecules or atoms, each of which is also capable of independent existence. For example, the organomonophosphite ligands employable herein possess a phosphorus donor atom having one available or unshared pair of electrons capable of forming a coordinate bond with the metal. Carbon monoxide, which is also properly classified as a ligand, can also be present and coordinated to the metal. The
30 ultimate composition of the complex catalyst may also contain an additional ligand, e.g., hydrogen or an anion satisfying the coordination sites or nuclear charge of the metal. Illustrative additional ligands include, for example, halogen (Cl, Br, I), alkyl, aryl, substituted aryl, acyl, CF₃, C₂F₅, CN, (R)₂PO and RP(O)(OH)O (wherein each R is the

same or different and is a substituted or unsubstituted hydrocarbon radical, e.g., the alkyl or aryl), acetate, acetylacetonate, SO₄, PF₄, PF₆, NO₂, NO₃, CH₃, CH₂=CHCH₂, CH₃CH=CHCH₂, C₆H₅CN, CH₃CN, NH₃, pyridine, (C₂H₅)₃N, mono-olefins, diolefins and triolefins, tetrahydrofuran, and the like. The complex species are preferably free of any
 5 additional organic ligand or anion that might poison the catalyst or have an undue adverse effect on catalyst performance. It is preferred in the rhodium-organomonophosphite ligand complex catalyzed hydroformylation reactions that the active catalysts be free of halogen and sulfur directly bonded to the metal, although such may not be absolutely necessary.

The organomonophosphite compounds that may serve as the ligand of the rhodium-
 10 organomonophosphite ligand complex catalyst and/or free ligand may be of the achiral (optically inactive) or chiral (optically active) type and are well known in the art. Achiral organomonophosphite ligands are preferred.

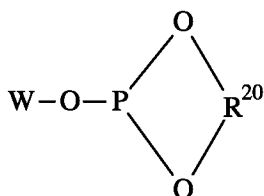
Representative organomonophosphites may include those having the formula:



<<I>>

15 wherein R¹⁰ represents a substituted or unsubstituted trivalent hydrocarbon radical containing from 4 to 40 carbon atoms or greater, such as trivalent acyclic and trivalent cyclic radicals, e.g., trivalent alkylene radicals such as those derived from 1,2,2-trimethylolpropane and the like, or trivalent cycloalkylene radicals such as those derived from 1,3,5-trihydroxycyclohexane, and the like. Such organomonophosphites may be found
 20 described in greater detail, for example, in US 4,567,306.

Representative organomonophosphites may include diorganomonophosphites such as those having the formula:



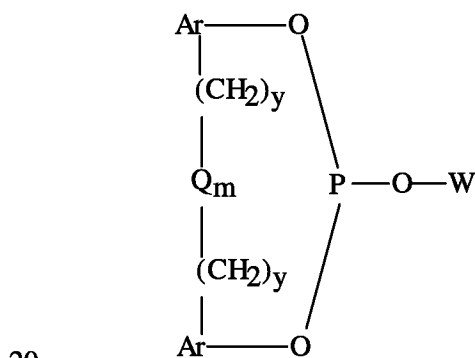
<<II>>

25 wherein R²⁰ represents a substituted or unsubstituted divalent hydrocarbon radical containing from 4 to 40 carbon atoms or greater and W represents a substituted or

unsubstituted monovalent hydrocarbon radical containing from 1 to 18 carbon atoms or greater.

Representative substituted and unsubstituted monovalent hydrocarbon radicals represented by W in the above Formula (II) include alkyl and aryl radicals, while
 5 representative substituted and unsubstituted divalent hydrocarbon radicals represented by R²⁰ include divalent acyclic radicals and divalent aromatic radicals. Illustrative divalent acyclic radicals include, for example, alkylene, alkylene-oxy-alkylene, alkylene-S-alkylene, cycloalkylene radicals, and, alkylene-NR²⁴-alkylene wherein R²⁴ is hydrogen or a substituted or unsubstituted monovalent hydrocarbon radical, e.g., an alkyl radical having 1
 10 to 4 carbon atoms. The more preferred divalent acyclic radicals are the divalent alkylene radicals such as disclosed more fully, for example, in U.S. Patent Nos. 3,415,906 and 4,567,302 and the like. Illustrative divalent aromatic radicals include, for example, arylene, bisarylene, arylene-alkylene, arylene-alkylene-arylene, arylene-oxy-arylene, arylene-NR²⁴-arylene wherein R²⁴ is as defined above, arylene-S-arylene, and arylene-S-alkylene, and the
 15 like. More preferably R²⁰ is a divalent aromatic radical such as disclosed more fully, for example, in U.S. Patent Nos. 4,599,206, 4,717,775, 4,835,299, and the like.

Representative of a more preferred class of diorganomonophosphites are those of the formula:



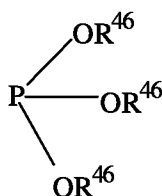
<<III>>

wherein W is as defined above, each Ar is the same or different and represents a substituted or unsubstituted aryl radical, each y is the same or different and is a value of 0 or 1, Q represents a divalent bridging group selected from -C(R³³)₂-, -O-, -S-, -NR²⁴-, Si(R³⁵)₂ and -CO-, wherein each R³³ is the same or different and represents hydrogen, an alkyl
 25 radical having from 1 to 12 carbon atoms, phenyl, tolyl, and anisyl, R²⁴ is as defined above, each R³⁵ is the same or different and represents hydrogen or a methyl radical, and m has a

value of 0 or 1. Such diorganomonophosphites are described in greater detail, for example, in U.S. Patent Nos. 4,599,206, 4,717,775, and 4,835,299.

Representative organomonophosphites may include triorganomonophosphites such as those having the formula:

5



<<IV>>

wherein each R⁴⁶ is the same or different and is a substituted or unsubstituted monovalent hydrocarbon radical e.g., an alkyl, cycloalkyl, aryl, alkaryl and aralkyl radicals that may contain from 1 to 24 carbon atoms. Illustrative triorganomonophosphites include, 10 for example, trialkyl phosphites, dialkylaryl phosphites, alkyl diaryl phosphites, triaryl phosphites, and the like, such as, for example, trimethyl phosphite, triethyl phosphite, butyldiethyl phosphite, tri-n-propyl phosphite, tri-n-butyl phosphite, tri-2-ethylhexyl phosphite, tri-n-octyl phosphite, tri-n-dodecyl phosphite, dimethylphenyl phosphite, diethylphenyl phosphite, methyl diphenyl phosphite, ethyl diphenyl phosphite, triphenyl 15 phosphite, trinaphthyl phosphite, bis(3,6,8-tri-t-butyl-2-naphthyl)methylphosphite, bis(3,6,8-tri-t-butyl-2-naphthyl)cyclohexylphosphite, tris(3,6-di-t-butyl-2-naphthyl)phosphite, bis(3,6,8-tri-t-butyl-2-naphthyl)(4-biphenyl)phosphite, bis(3,6,8-tri-t-butyl-2-naphthyl)phenylphosphite, bis(3,6,8-tri-t-butyl-2-naphthyl)(4-benzoylphenyl)phosphite, bis(3,6,8-tri-t-butyl-2-naphthyl)(4-sulfonylphenyl)phosphite, and 20 the like. A preferred triorganomonophosphite is tris(2,4-di-t-butylphenyl)phosphite. Such triorganomonophosphites are described in greater detail, for example, in U.S. Patent Nos. 3,527,809 and 4,717,775.

As noted above, the metal-organomonophosphite ligand complex catalysts may be formed by methods known in the art. For instance, preformed rhodium hydrido-carbonyl- 25 organomonophosphite ligand catalysts may be prepared and introduced into the reaction mixture of a hydroformylation process. More preferably, the rhodium-organomonophosphite ligand complex catalysts can be derived from a rhodium catalyst precursor that may be introduced into the reaction medium for in situ formation of the active catalyst. For example, rhodium catalyst precursors such as rhodium dicarbonyl 30 acetylacetonate, Rh₂O₃, Rh₄(CO)₁₂, Rh₆(CO)₁₆, Rh(NO₃)₃, and the like may be introduced

into the reaction mixture along with the organomonophosphite ligand for the in situ formation of the active catalyst. In some embodiments, rhodium dicarbonyl acetylacetonate is employed as a rhodium precursor and combined in the presence of a solvent with the organomonophosphite ligand to form a catalytic rhodium-organomonophosphite ligand complex precursor that is introduced into the reactor along with excess (free) organomonophosphite ligand for the in situ formation of the active catalyst. In any event, it is sufficient for the purposes of this invention that carbon monoxide, hydrogen and organomonophosphite ligand compound are all ligands that are capable of being complexed with the metal and that an active metal-organomonophosphite ligand catalyst is present in the reaction mixture under the conditions used in the hydroformylation reaction. Carbonyl and organomonophosphite ligands, if not already complexed with the initial rhodium, may be complexed to the rhodium either prior to, or in situ during the hydroformylation process.

By way of illustration, an exemplary catalyst precursor composition for use in some embodiments consists essentially of a solubilized rhodium carbonyl organomonophosphite ligand complex precursor, a solvent and, optionally, free organomonophosphite ligand. The preferred catalyst precursor composition can be prepared by forming a solution of rhodium dicarbonyl acetylacetonate, an organic solvent and a organomonophosphite ligand. The organomonophosphite ligand readily replaces one of the carbonyl ligands of the rhodium acetylacetonate complex precursor at room temperature as witnessed by the evolution of carbon monoxide gas. This substitution reaction may be facilitated by heating the solution if desired. Any suitable organic solvent in which both the rhodium dicarbonyl acetylacetonate complex precursor and rhodium organomonophosphite ligand complex precursor are soluble can be employed. The amounts of rhodium complex catalyst precursor, organic solvent and organomonophosphite ligand, as well as their preferred embodiments present in such catalyst precursor compositions may obviously correspond to those amounts employable in the hydroformylation process of this invention. Experience has shown that the acetylacetonate ligand of the precursor catalyst is replaced after the hydroformylation process has begun with a different ligand, e.g., hydrogen, carbon monoxide or organomonophosphite ligand, to form the active complex catalyst as explained above. The acetylacetonate that is freed from the precursor catalyst under hydroformylation conditions is removed from the reaction medium with the product aldehyde and thus is in no way detrimental to the hydroformylation process. The use of such rhodium complex

catalytic precursor compositions provides a simple economical and efficient method for handling the rhodium precursor and hydroformylation start-up.

Accordingly, the metal-organomonophosphite ligand complex catalyst used in the process of this invention consists essentially of the metal complexed with carbon monoxide and a organomonophosphite ligand, said ligand being bonded (complexed) to the metal. Moreover, the terminology "consists essentially of", as used herein, does not exclude, but rather includes, hydrogen complexed with the metal, in addition to carbon monoxide and the organomonophosphite ligand. Further, such terminology does not exclude the possibility of other organic ligands and/or anions that might also be complexed with the metal. Materials in amounts that unduly adversely poison or unduly deactivate the catalyst are not desirable and so the catalyst most desirably is free of contaminants such as metal-bound halogen (e.g., chlorine, and the like) although such may not be absolutely necessary. The hydrogen and/or carbonyl ligands of an active metal-organomonophosphite ligand complex catalyst may be present as a result of being ligands bound to a precursor catalyst and/or as a result of in situ formation, e.g., due to the hydrogen and carbon monoxide gases employed in hydroformylation process.

As noted, the hydroformylation process of this invention involves the use of a metal-organomonophosphite ligand complex catalyst as described herein. Mixtures of such catalysts can also be employed if desired. The amount of metal-organomonophosphite ligand complex catalyst present in the reaction fluid of a given hydroformylation process encompassed by this invention need only be that minimum amount necessary to provide the given metal concentration desired to be employed and that will furnish the basis for at least the catalytic amount of metal necessary to catalyze the particular hydroformylation process involved such as disclosed, for example, in the above-mentioned patents. In general, catalytic metal, e.g., rhodium, concentrations in the range of from 50 ppmw to 1000 ppmw, calculated as free metal in the reaction medium, should be sufficient for most processes, while it is generally preferred to employ from 100 to 500 ppmw of metal. Analytical techniques for measuring catalytic metal concentrations are well known to the skilled person, and include atomic absorption (AA), inductively coupled plasma (ICP) and X-ray fluorescence (XRF); AA is typically preferred.

In addition to the metal-organomonophosphite ligand complex catalyst, free organomonophosphite ligand (i.e., ligand that is not complexed with the metal) may also be present in the reaction medium. The free organomonophosphite ligand may correspond to

any of the above-defined organomonophosphite ligands discussed above as employable herein. It is preferred that the free organomonophosphite ligand be the same as the organomonophosphite ligand of the metal-organomonophosphite ligand complex catalyst employed. However, such ligands need not be the same in any given process. The hydroformylation process may involve from 0.1 moles or less to 100 moles or higher of free organomonophosphite ligand per mole of metal in the reaction medium. Preferably, the hydroformylation process is carried out in the presence of from 1 to 50 moles of free organomonophosphite ligand per mole of metal present in the reaction medium. The concentration of organomonophosphite is typically measured by high pressure liquid chromatography (HPLC) or ^{31}P NMR spectroscopy. Since it is more preferred to produce non-optically active aldehydes by hydroformylating achiral olefins, the more preferred organomonophosphite ligands are achiral type organomonophosphite ligands, especially those encompassed by Formula (I-IV) above. If desired, make-up or additional organomonophosphite ligand can be supplied to the reaction medium of the hydroformylation process at any time and in any suitable manner, e.g. to maintain a predetermined level of free ligand in the reaction medium.

The hydroformylation products may be asymmetric, non-asymmetric or a combination thereof, with the preferred products being non-asymmetric. The process may be conducted in any batch, continuous or semi-continuous fashion and in some embodiments, involves a catalyst liquid recycle operation.

The liquid recycle procedure generally involves withdrawing a portion of the liquid reaction medium containing the catalyst and aldehyde product from the hydroformylation reactor, i.e., reaction zone, either continuously or intermittently, and recovering the aldehyde product therefrom by distilling it, i.e. vaporization separation, in one or more stages under normal, reduced or elevated pressure, as appropriate, in a separate distillation zone, the non-volatilized metal catalyst containing residue being recycled to the reaction zone as disclosed, for example, in U.S. Patent No. 5,288,918, U.S. Patent No. 8,404,903, and U.S. Patent No. 10,023,516. Condensation of the volatilized materials, and separation and further recovery thereof, e.g., by further distillation, can be carried out in any conventional manner, the crude aldehyde product can be passed on for further purification and isomer separation, if desired.

Unreacted olefinic starting material may be separated from the product aldehydes by conventional means, for example, by distillation. The olefin thus recovered may then be

recycled back to the reaction zone, or may be added to the reaction fluid at one or more locations between the reaction zone and the strip gas vaporizer.

The hydroformylation reaction mixture compositions employable herein can and normally will contain minor amounts of additional ingredients such as those that have either
5 been deliberately employed in the hydroformylation process or formed in situ during said process. Examples of such ingredients that can also be present include unreacted olefin starting material, carbon monoxide and hydrogen gases, and in situ formed type products, such as saturated hydrocarbons and/or unreacted isomerized olefins corresponding to the olefin starting materials, ligand degradation compounds, and high boiling liquid aldehyde
10 condensation by-products, as well as other inert co-solvent type materials or hydrocarbon additives, if employed.

The reaction conditions of the hydroformylation process encompassed by this invention may include any suitable hydroformylation conditions heretofore employed for producing optically active and/or non-optically active aldehydes. For instance, the total gas
15 pressure of hydrogen, carbon monoxide and olefin starting compound of the hydroformylation process may range from 1 to 69,000 kPa. In general, however, it is preferred that the process be operated at a total gas pressure of hydrogen, carbon monoxide and olefin starting compound of less than 14,000 kPa and more preferably less than 3,400 kPa. The minimum total pressure is limited predominantly by the amount of reactants
20 necessary to obtain a desired rate of reaction. More specifically, the carbon monoxide and hydrogen partial pressures may each independently range from 1 to 6,900 kPa, and preferably from 34 to 3,400 kPa. In general, H₂:CO molar ratio of gaseous hydrogen to carbon monoxide in a reaction zone may range from 1:10 to 100:1 or higher, the more preferred hydrogen to carbon monoxide molar ratio being from 1:10 to 10:1.

25 In general, the hydroformylation process may be conducted at any operable reaction temperature. Hydroformylation reaction temperatures of 70 °C to 120 °C are generally preferred for branched internal olefinic starting materials. It is to be understood that when non-optically active aldehyde products are desired, achiral type olefin starting materials and organomonophosphite ligands are employed and when optically active aldehyde products
30 are desired prochiral or chiral type olefin starting materials and organomonophosphite ligands are employed. The hydroformylation reaction conditions employed will be governed by the type of aldehyde product desired.

The hydroformylation process of this invention may be carried out using one or more suitable reactors such as, for example, a fixed bed reactor, a tubular reactor, a venturi reactor, a bubble column reactor, a continuous stirred tank reactor (CSTR) or a slurry reactor. The optimum size and shape of the reactor will depend on the type of reactor used.

5 The at least one reaction zone employed in this invention may be a single vessel or may comprise two or more discrete vessels.

The hydroformylation process of this invention is conducted in a continuous fashion, with the recycle of unconsumed starting materials. The reaction can be conducted in a single reaction zone or in a plurality of reaction zones, in series or in parallel. The materials

10 of construction employed should be substantially inert to the starting materials during the reaction and the fabrication of the equipment should be able to withstand the reaction temperatures and pressures. Means to introduce and/or adjust the quantity of starting materials or ingredients introduced continuously into the reaction zone during the course of the reaction can be conveniently utilized in the process especially to maintain the desired

15 molar ratio of the starting materials. The starting materials and/or recycled olefin may be added to each or all the reaction zones in series.

The hydroformylation process may be conducted in either glass lined, stainless steel or similar type reaction equipment. The reaction zone may be fitted with one or more internal and/or external heat exchanger(s) in order to control undue temperature

20 fluctuations, or to prevent any possible "runaway" reaction temperatures.

The hydroformylation process of this invention may be conducted in one or more steps or stages. The exact number of reaction steps or stages will be governed by the best compromise between capital costs and achieving high catalyst selectivity, activity, lifetime and ease of operability, as well as the intrinsic reactivity of the starting materials in question

25 and the stability of the starting materials and the desired reaction product to the reaction conditions.

In an embodiment, the hydroformylation may be carried out in a multistaged reactor such as described, for example, in U.S. Patent No. 5,728,893. Such multistaged reactors can be designed with internal, physical barriers that create more than one theoretical

30 reactive stage per vessel. In effect, it is like having a number of reactors inside a single continuous stirred tank reactor vessel. Multiple reactive stages within a single vessel is a cost effective way of using the reactor vessel volume. It significantly reduces the number of

vessels that otherwise would be required to achieve the same results. Fewer vessels reduces the overall capital required and maintenance concerns with separate vessels and agitators.

A typical hydroformylation process using a metal-organomonophosphite ligand complex catalyst is carried out in a continuous manner and comprises: (a) feeding mixed C8 olefins, carbon monoxide and hydrogen to a reaction zone containing a reaction fluid, where
5 the reaction fluid comprises a solvent, the metal-organomonophosphite ligand complex catalyst, and free organomonophosphite ligand; (b) maintaining reaction temperature and pressure conditions favorable to the hydroformylation of the olefinic starting material(s); (c) supplying make-up quantities of the mixed C8 olefins (including recycled olefins), carbon
10 monoxide, and hydrogen to the reaction zone as those reactants are consumed; (d) separating the desired product aldehyde(s) from the reaction fluid in a separation zone; (e) maintaining an average branched olefin concentration of at least 2% by weight within the reaction fluid during the separation step; (f) recovering unreacted olefins from the crude product aldehyde(s) by a distillation, (f) returning at least a portion of the unreacted olefins
15 to the reaction zone; and, optionally (g) adding additional rhodium and/or organomonophosphite ligand to maintain target concentrations.

General examples of liquid recycle hydroformylation processes are well known in the art and involve returning the metal-ligand complex catalyst fluid separated from the desired aldehyde reaction product(s) to one or more reaction zones, such as disclosed, for
20 example in U.S. Patent Nos. 4,148,830; 4,668,651; 4,774,361; 5,102,505 and 5,110,990.

Separation of the desired aldehyde product from the metal-organomonophosphite complex catalyst containing reaction fluid may take place at any suitable temperature desired. In general, it is preferred that such separation take place at relatively low temperatures, such as below 150 °C, and more preferably at a temperature in the range of
25 from 50 °C to 140 °C.

Embodiments of hydroformylation processes of the present invention utilize a strip gas vaporizer in the separation zone such as is described for example in U.S. Patent No. 8,404,903 and U.S. Patent No. 10,023,516. In such an embodiment, the reaction fluid is introduced to a vaporizer at elevated temperature along with a stream of flowing gas
30 comprising carbon monoxide and optionally hydrogen and nitrogen (strip gas), which becomes saturated with volatile components comprising product aldehydes and unreacted olefins. The gaseous stream exits the vaporizer and passes through a condenser (a “strip gas condenser”) to generate a liquid, crude product stream comprised of product aldehydes and

olefins, and a gaseous stream comprised of carbon monoxide, residual product aldehydes and olefins which remained in the gaseous phase after passing through the strip gas condenser. At least a portion of the gaseous stream is recycled and incorporated into the strip gas using a compressor or blower (recycle gas). The concentration of components that
5 may be condensed at moderate temperatures and pressures such as unreacted olefins in the strip gas is determined in part by the temperature of the strip gas condenser. For example, lowering the temperature of the strip gas condenser will result in more condensable components being removed from the gaseous stream as liquids, thereby lowering their concentration in the recycle gas. Conversely, raising the strip gas condenser temperature
10 will result in a higher concentration of condensable components returning to the vaporizer in the recycle gas.

In one embodiment, the separation zone comprises a carbon monoxide (CO) strip gas vaporizer such as is described in U.S. Patent No. 10,023,516; such an embodiment employs a strip gas rich in CO.

15 The ratio of the mass of reaction fluid entering the strip gas vaporizer (feed) to the mass of the non-volatilized catalyst-containing fluid leaving the strip gas vaporizer (tails) is maintained within a range of greater than 1 to 3. If this feed to tails ratio is too high (e.g. \geq 4), the catalyst will become highly concentrated within the strip gas vaporizer which may exacerbate rhodium loss. Conversely, if the feed to tails ratio is too low, the rate of
20 aldehyde removal will limit production rates. A feed to tails ratio of 1.5 to 3 is used in some embodiments. In some embodiments, a feed to tails ratio of 1.9 to 2.5 is used.

Processes of the present invention can advantageously improve rhodium
25 accountability in continuous liquid recycle hydroformylation processes in which mixed C8 olefins or mixed C9 olefins are hydroformylated in the presence of rhodium-organomonophosphate catalyst compositions. In prior reaction processes, the measured concentration of rhodium in a reaction fluid has been observed as declining over time. The concentration of rhodium can be measured using a variety of techniques including, for example, atomic absorption (AA) and inductively coupled plasma (ICP). Unless otherwise
30 specified herein or in the claims, the amount of rhodium in a fluid is measured using atomic absorption. In using processes of the present invention, the rate at which the concentration of rhodium declines in a reaction is slower using the inventive process than observed in

typical processes for the hydroformylation of mixed C8 olefins or mixed C9 olefins using rhodium and an organomonophosphite ligand.

In one aspect, a process to improve rhodium accountability in a continuous liquid recycle hydroformylation process comprises contacting in a reaction zone reactants
5 comprising mixed C8 olefins, hydrogen, and carbon monoxide in the presence of a catalyst comprising rhodium and an organomonophosphite ligand to form a reaction fluid, wherein the reaction fluid is introduced to a strip gas vaporizer to produce a product stream and a vaporizer tails stream, and wherein the vaporizer tails stream comprises at least 1.2 percent by weight C8 internal olefins. In some embodiments, the vaporizer tails stream comprises
10 at least 1.4 percent by weight C8 internal olefins. The vaporizer tails stream comprises up to 20 percent by weight C8 internal olefins in some embodiments. In some embodiments, the vaporizer tails stream comprises 1.4 to 15 percent by weight C8 internal olefins, or 1.4 to 10 percent by weight C8 internal olefins.

The step of contacting in a reaction zone reactants comprising mixed C8 olefins,
15 hydrogen, and carbon monoxide in the presence of a catalyst comprising rhodium and an organomonophosphite ligand to form a reaction fluid can be conducted as described herein. Without wishing to be bound by any particular theory, maintaining a certain concentration of C8 internal olefins in the vaporizer tails stream from a strip gas vaporizer is believed to improve the rhodium accountability in the process (i.e., the rate at which the rhodium
20 concentration decreases in the reaction fluid decreases).

In some embodiments, the C8 internal olefin concentration in the vaporizer tails stream is increased. For example, in order to maintain the concentration of C8 internal olefins in the vaporizer tails stream above 1.2 percent by weight, adjustments may be needed to increase the C8 internal olefin concentration. In various embodiments, the C8
25 internal olefin concentration in the vaporizer tails may be increased by one or more of: (a) increasing the C8 internal olefin concentration in the reaction fluid entering the strip gas vaporizer; or (b) lowering the heavies concentration in the reaction fluid entering the strip gas vaporizer; or (c) lowering the ratio of the mass of reaction fluid fed to the strip gas vaporizer to the mass of the vaporizer tails stream; or (d) raising the temperature of a strip
30 gas condenser associated with the strip gas vaporizer. Thus, if the C8 internal olefin concentration in the vaporizer tails stream begins to fall below the target value, one or more of these corrective actions may be taken to increase it. The concentration of C8 internal

olefin may be determined by gas chromatography (GC) using the method described in the Examples section.

In one embodiment, the C8 internal olefin concentration in the vaporizer tails stream may be increased by increasing the concentration of C8 internal olefins in the reaction fluid being fed to the strip gas vaporizer, which may be accomplished by decreasing the hydroformylation rate in the reaction zone. Methods of determining the hydroformylation rate in a reaction zone are well-known to those of ordinary skill in the art, and include but are not limited to calculating a turn over frequency (moles of aldehydes produced per mole of rhodium per unit time). The hydroformylation rate may be reduced in a number of ways including, for example by lowering the reaction temperature, changing the CO or H₂ partial pressures, or reducing the rhodium concentration. While normally a lower conversion would not be desirable, because the olefin will be recycled in the present process, the hydroformylation conversion on a single pass through the reaction zone may not be as important as avoiding rhodium loss.

In some embodiments, the concentration of C8 internal olefins in the reaction fluid being fed to the strip gas vaporizer (which increases the C8 internal olefin concentration in the vaporizer tails stream) may be increased by reducing olefin conversion in the reactor(s). For example, olefin conversion in one or more reaction zones may be reduced by one or more of a) lowering the residence time of the reaction fluid within the reaction zone(s), b) increasing the mixed C8 olefin feed rate, c) increasing the feed of recycled olefins to the reaction zone(s), and d) increasing the proportion of recycled olefin being fed to the reaction zone(s). For convenience, the recycled olefin may be combined with the mixed C8 olefin comprising the primary feed. As stated above, recycled olefins are comprised of dimethyl hexenes which hydroformylate more slowly than linear octenes or methyl heptenes such that olefin conversion will decline as the concentration of recycled olefin increases.

In some embodiments, the concentration of C8 internal olefins in the reaction fluid being fed to the strip gas vaporizer (which increases the C8 internal olefin concentration in the vaporizer tails stream) may be increased by adding mixed C8 olefin or recycled olefin to the reaction fluid between the reaction zone and the separation zone. For example, if the reaction zone comprises a series of stirred vessels, and the C8 internal olefin concentration in the reaction fluid leaving the final reaction vessel is less than desired, mixed C8 or recycled olefin may be added to the reaction fluid before it enters the separation zone.

Alternatively, the recycled olefin may be added to any one or more of the reactors in series (e.g., the last one). A combination of mixed C8 and recycled olefin may be used.

In some embodiments, the C8 internal olefin concentration in the vaporizer tails stream may be increased by lowering the heavies concentration in the reaction fluid entering the strip gas vaporizer. For example, the reaction fluid entering the strip gas vaporizer contains olefins and heavies, with the balance comprising aldehydes. If the heavies concentration is lowered, the concentration of aldehydes in the reaction fluid entering the separation zone will increase, which will result in a higher partial pressure of aldehydes in the separation zone. A higher partial pressure of product aldehydes in the separation zone will allow production rates to be achieved at lower temperatures and/or higher pressures in the separation zone; these milder conditions will also slow the rate of C8 internal olefin removal and thereby increase their concentration in the reaction fluid within the strip gas vaporizer and by extension, their concentration in the vaporizer tails stream. The heavies concentration in the reaction fluid may be lowered by purging a portion of the vaporizer tails; the fluid thus removed may be processed to recover rhodium.

In some embodiments, the C8 internal olefin concentration in the vaporizer tails stream may be increased by raising the temperature of a strip gas condenser associated with the strip gas vaporizer. Such an action will reduce condensation of the C8 internal olefins, thereby increasing their concentration in the recycle gas which will reduce the rate at which the strip gas will remove C8 internal olefins from the reaction fluid as it travels through the strip gas vaporizer. Measuring the concentration of C8 internal olefins in the vaporizer tails stream will allow adjustments in the strip gas condenser temperature to be made as needed.

In some embodiments, the C8 internal olefin concentration in the vaporizer tails stream may be increased by lowering the ratio of the mass of reaction fluid fed to the strip gas vaporizer to the mass of the vaporizer tails stream (i.e., lowering the feed to tails ratio). This may be accomplished by a process comprising one or more of a) increasing the temperature in the strip gas vaporizer, b) increasing the pressure in the strip gas vaporizer, c) decreasing the strip gas flow rate, or d) increasing the mass of reaction fluid entering the separation zone per unit time.

In some embodiments, a combination of two or more adjustments may be made to reach the target of a C8 internal olefin concentration in the vaporizer tails stream of at least 1.2 wt. %. For example, a combination of a) increasing the C8 internal olefin concentration in the reaction fluid entering the strip gas vaporizer (e.g., slowing the hydroformylation rate

and/or limiting olefin conversion in the reaction zone), and/or b) lowering the heavies concentration in the reaction fluid entering the strip gas vaporizer, and/or c) lowering the ratio of the mass of reaction fluid fed to the strip gas vaporizer to the mass of the vaporizer tails stream, and/or d) raising the temperature of a strip gas condenser associated with the strip gas vaporizer.

Some embodiments further comprise removing olefins from the product stream and returning the removed olefins to the reaction fluid before introduction into the strip gas vaporizer.

Accordingly, illustrative aldehyde products include n-nonanal, 2-methyloctanal, 3-methyloctanal, 4-methyloctanal, 5-methyloctanal, 6-methyloctanal, 7-methyloctanal, 2-ethylheptanal, 2-propylhexanal, 3-propylhexanal, 4,5-dimethylheptanal, 2,3,4-trimethylhexanal, 3-ethyl-4-methylhexanal, 2-ethyl-4-methylheptanal, 2-propyl-3-methylpentanal, 2,5-dimethylheptanal, 2,3-dimethylheptanal, and the like.

In other embodiments, mixed C9 olefins are hydroformylated. In one such aspect, a process to improve rhodium accountability in a continuous liquid recycle hydroformylation process comprises contacting in a reaction zone reactants comprising mixed C9 olefins, hydrogen, and carbon monoxide in the presence of a catalyst comprising rhodium and an organomonophosphate ligand to form a reaction fluid, wherein the reaction fluid is introduced to a strip gas vaporizer to produce a product stream and a vaporizer tails stream, and wherein the vaporizer tails stream comprises at least 1.3 percent by weight C9 internal olefins. In some embodiments, the vaporizer tails stream comprises at least 1.4 percent by weight C9 internal olefins. The vaporizer tails stream comprises up to 20 percent by weight C9 internal olefins in some embodiments. In some embodiments, the vaporizer tails stream comprises 1.4 to 15 percent by weight C9 internal olefins, or 1.4 to 10 percent by weight C9 internal olefins.

The step of contacting in a reaction zone reactants comprising mixed C9 olefins, hydrogen, and carbon monoxide in the presence of a catalyst comprising rhodium and an organomonophosphate ligand to form a reaction fluid can be conducted as described herein. Without wishing to be bound by any particular theory, maintaining a certain concentration of C9 internal olefins in the vaporizer tails stream from a strip gas vaporizer is believed to improve the rhodium accountability in the process (i.e., the rate at which the rhodium concentration decreases in the reaction fluid decreases).

In some embodiments, the C9 internal olefin concentration in the vaporizer tails stream is increased. For example, in order to maintain the concentration of C9 internal olefins in the vaporizer tails stream above 1.3 percent by weight, adjustments may be needed to increase the C9 internal olefin concentration. In various embodiments, the C9 internal olefin concentration in the vaporizer tails may be increased by one or more of: (a) increasing the C9 internal olefin concentration in the reaction fluid entering the strip gas vaporizer; or (b) lowering the heavies concentration in the reaction fluid entering the strip gas vaporizer; or (c) lowering the ratio of the mass of reaction fluid fed to the strip gas vaporizer to the mass of the vaporizer tails stream; or (d) raising the temperature of a strip gas condenser associated with the strip gas vaporizer. Thus, if the C9 internal olefin concentration in the vaporizer tails stream begins to fall below the target value, one or more of these corrective actions may be taken to increase it. The concentration of C9 internal olefin may be determined by gas chromatography (GC) using the method described in the Examples section.

In one embodiment, the C9 internal olefin concentration in the vaporizer tails stream may be increased by increasing the concentration of C9 internal olefins in the reaction fluid being fed to the strip gas vaporizer. The concentration of C9 internal olefins in the reaction fluid being fed to the strip gas vaporizer may be increased by decreasing the hydroformylation rate in the reaction zone. Methods of determining the hydroformylation rate in a reaction zone are well-known to those of ordinary skill in the art, and include but are not limited to calculating a turn over frequency (moles of aldehydes produced per mole of rhodium per unit time). The hydroformylation rate may be reduced in a number of ways including, for example by lowering the reaction temperature, changing the CO or H₂ partial pressures, or reducing the rhodium concentration. While normally a lower conversion would not be desirable, because the olefin will be recycled in the present process, the hydroformylation conversion on a single pass through the reaction zone may not be as important as avoiding rhodium loss.

In some embodiments, the concentration of C9 internal olefins in the reaction fluid being fed to the strip gas vaporizer (which increases the C9 internal olefin concentration in the vaporizer tails stream) may be increased by reducing olefin conversion in the reactor(s). For example, olefin conversion in one or more reaction zones may be reduced by one or more of a) lowering the residence time of the reaction fluid within the reaction zone(s), b) increasing the mixed C9 olefin feed rate, c) increasing the feed of recycled olefins to the

reaction zone(s), and d) increasing the proportion of recycled olefin being fed to the reaction zone(s). For convenience, the recycled olefin may be combined with the mixed C9 olefin comprising the primary feed.

In some embodiments, the concentration of C9 internal olefins in the reaction fluid being fed to the strip gas vaporizer (which increases the C9 internal olefin concentration in the vaporizer tails stream) may be increased by adding mixed C9 olefin or recycled olefin to the reaction fluid between the reaction zone and the separation zone. For example, if the reaction zone comprises a series of stirred vessels, and the C9 internal olefin concentration in the reaction fluid leaving the final reaction vessel is less than desired, mixed C9 or recycled olefin may be added to the reaction fluid before it enters the separation zone. Alternatively, the recycled olefin may be added to any one or more of the reactors in series (e.g., the last one). A combination of mixed C9 and recycled olefin may be used.

In some embodiments, the C9 internal olefin concentration in the vaporizer tails stream may be increased by lowering the heavies concentration in the reaction fluid entering the strip gas vaporizer. For example, the reaction fluid entering the strip gas vaporizer contains olefins and heavies, with the balance comprising aldehydes. If the heavies concentration is lowered, the concentration of aldehydes in the reaction fluid entering the separation zone will increase, which will result in a higher partial pressure of aldehydes in the separation zone. A higher partial pressure of product aldehydes in the separation zone will allow production rates to be achieved at lower temperatures and/or higher pressures in the separation zone; these milder conditions will also slow the rate of C9 internal olefin removal and thereby increase their concentration in the reaction fluid within the strip gas vaporizer and by extension, their concentration in the vaporizer tails stream. The heavies concentration in the reaction fluid may be lowered by purging a portion of the vaporizer tails; the fluid thus removed may be processed to recover rhodium.

In some embodiments, the C9 internal olefin concentration in the vaporizer tails stream may be increased by raising the temperature of a strip gas condenser associated with the strip gas vaporizer. Such an action will reduce condensation of the C9 internal olefins, thereby increasing their concentration in the recycle gas which will reduce the rate at which the strip gas will remove C9 internal olefins from the reaction fluid as it travels through the strip gas vaporizer. Measuring the concentration of C9 internal olefins in the vaporizer tails stream will allow adjustments in the strip gas condenser temperature to be made as needed.

In some embodiments, the C9 internal olefin concentration in the vaporizer tails stream may be increased by lowering the ratio of the mass of reaction fluid fed to the strip gas vaporizer to the mass of the vaporizer tails stream (i.e., lowering the feed to tails ratio). This may be accomplished by a process comprising one or more of a) increasing the
 5 temperature in the strip gas vaporizer, b) increasing the pressure in the strip gas vaporizer, c) decreasing the strip gas flow rate, or d) increasing the mass of reaction fluid entering the separation zone per unit time.

In some embodiments, a combination of two or more adjustments may be made to reach the target of a C9 internal olefin concentration in the vaporizer tails stream of at least
 10 1.3 wt. %. For example, a combination of a) increasing the C9 internal olefin concentration in the reaction fluid entering the strip gas vaporizer (e.g., slowing the hydroformylation rate and/or limiting olefin conversion in the reaction zone), and/or b) lowering the heavies concentration in the reaction fluid entering the strip gas vaporizer, and/or c) lowering the ratio of the mass of reaction fluid fed to the strip gas vaporizer to the mass of the vaporizer
 15 tails stream, and/or d) raising the temperature of a strip gas condenser associated with the strip gas vaporizer.

Some embodiments further comprise removing olefins from the product stream and returning the removed olefins to the reaction fluid before introduction into the strip gas vaporizer.

20 Some embodiments of the invention will now be described in more detail in the following Examples.

EXAMPLES

All parts and percentages in the following examples are by weight unless otherwise indicated. Pressures are given as absolute pressure unless otherwise indicated.

25 Olefin compositions are determined by gas chromatography (GC) using the following parameters:

Column – Petrocol DH 100 m X 0.25 mm; 0.5 μ film
Injection – 1 μ L; split ratio 150 : 1
Detector – FID at 270 °C
Oven program – 40 °C for 40 minutes, to 220 °C at 10 °C/min; hold 5 min, to 260 °C at 5 °C/min; hold 19 minutes, to 270 °C; hold 48 minutes.

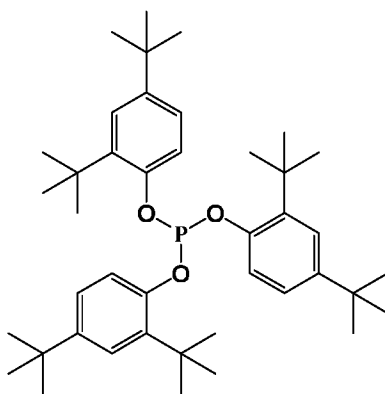
Component quantitation is based on external standard calibration; the multiple linear octene, dimethyl hexene and methyl heptene isomers are grouped for reporting purposes.

Rhodium concentration is measured by atomic absorption spectroscopy (AA) using a Perkin Elmer PinAAcle 900F with air-acetylene flame.

Olefin A comprises 25 weight % methyl heptenes and 62 weight % dimethyl hexenes with the balance comprising paraffins. The composition of Olefin A is
5 representative of unreacted olefins which are recovered from a product stream entering a separation zone (e.g., a strip gas vaporizer) and recycled to the reaction zone.

Rhodium is added as dicarbonyl(acetylacetonato)rhodium (I).

Ligand A is tris(2,4-di-tert-butylphenyl) phosphite which has the following structure:



10

Ligand A

Examples 1-7 use an accelerated testing procedure, referred to herein as the block-in procedure to demonstrate the impact of the separation zone on the catalyst. Said testing procedure involves subjecting solubilized activated rhodium complex catalysts to high
15 temperatures and low partial pressures of syn gas for a much longer period of time than would be experienced during a normal continuous liquid recycle hydroformylation process in order to obtain meaningful results in a practical fashion. For instance, the rhodium loss as discussed herein that may occur during a continuous liquid recycle hydroformylation
20 process may take weeks to define quantitatively under normal aldehyde distillative recovery procedures because the catalyst is subjected to such vaporizer conditions for only a matter of minutes each day, whereas the accelerated test (block-in procedure) can be completed within hours or days by continuously maintaining the reaction product fluid at high aldehyde recovery type distillation temperatures for a prolonged period of time. Block-in
25 segments comprise periods of time wherein the reactor is sealed under high temperatures and low syn gas partial pressures. This procedure is intended to simulate the effect of the separation zone on the catalyst solution.

Comparative Experiment A. A Fischer-Porter tube immersed in an oil bath at 115 °C is charged with tetraglyme (10 mL) under an atmosphere of nitrogen. Ligand A (1.7 wt %; 10 moles per mole of rhodium) and rhodium are added as stock solutions in toluene, and carbon monoxide and hydrogen are each sparged through the solution at a rate of 15 standard L/hr for about 1 hour, during which time the tube pressure is maintained at 164 psi [1.13MPa]. The gas flow is changed to nitrogen, and the solution is sparged at 10 standard L/hr while maintaining 164 psi [1.13MPa]. After 30 minutes, the tube is sealed, and the total pressure is lowered to 115 psi [0.793MPa]. The temperature is maintained at 115 °C, and the solution is sampled periodically for rhodium analysis.

Example 1-3. The procedure of Comparative Experiment A is followed, with the exception of the addition of varying amounts of Olefin A immediately prior to reducing the pressure and sealing the tube.

The amount of rhodium in the solution is measured initially, after 2 days, and after 5 days. The final rhodium accountability is calculated by the following:

15

Table 1

	Rhodium (ppmw)				final rhodium accountability (%)
	C8 internal olefins (wt %)	initial	after 2 days	after 5 days	
Comparative Experiment A	0	283	277	239	84
Example 1	4.5	256	259	261	102
Example 2	6.6	253	254	254	100
Example 3	8.6	254	252	249	98
Example 4	10.0	256	NA	239	93

The results of Table 1 show that the rhodium accountability is enhanced by the presence of ≥ 4.5 wt % C8 internal olefins.

Comparative Experiment B. The procedure of Comparative Experiment A is followed.

Examples 4-7. The procedure of Examples 1-3 is followed with the exception of the amount of Olefin A being added.

The amount of rhodium in the solution is measured initially, after 2 days, and after 5 days. Results for Comparative Experiment B and Examples 4-7 are summarized in Table 2.

25

Table 2

	total C8 internal olefins (wt %)	rhodium (ppmw)			final rhodium accountability (%)	final appearance
		initial	2 days	5 days		
Comparative Experiment B	0	315	59	36	12	dark precipitate, dark film
Example 4	2.1	326	316	280	86	clear orange, film
Example 5	2.5	331	322	275	83	clear orange, light film
Example 6	2.9	315	323	285	90	clear orange, no film
Example 7	3.4	307	295	300	98	clear yellow, no film

The results of Table 2 indicate that the presence of greater than 2 wt % total C8 internal olefins improves rhodium accountability. The appearance of the solution is an additional qualitative indication of rhodium stability; for example, a darkening of color of the formation of precipitate or film indicates that rhodium clustering is occurring.

Example 8. A model suitable for determining the average olefin concentration in a reaction fluid within a strip gas vaporizer is constructed using Aspen Plus Process Simulation software. The model comprises 5 flash blocks to simulate the change in concentration as the fluid travels down the vaporizer. The outlet temperature of the last flash block is set to 100 °C, while the outlet temperatures of the remaining flash blocks are adjusted to allow all of the blocks to perform equal duty. Total strip gas flow is adjusted to achieve the target feed to tails ratio (2:1). The strip gas condenser temperature is set to 20 °C; thus the recycle gas is saturated with both C9 aldehyde and C8 internal olefin at that temperature. The strip gas is pre-heated to 70 °C prior to entering the vaporizer. Calculations are performed for a solution comprising C8 internal olefin at 10 wt. %, C9 aldehyde trimer at 30 wt. %) and nonanal (balance), and the solution is fed to a strip gas vaporizer at 100 °C and 22 psi [0.15MPa].

Example 9. The procedure of Example 8 is followed with the exception of the strip gas condenser temperature being set to 30 °C.

Example 10. The procedure of Example 8 is followed with the exception of the strip gas condenser temperature being set to 40 °C.

Example 11. The procedure of Example 8 is followed with the exception of the strip gas condenser temperature being set to 50 °C.

Example 12. The procedure of Example 8 is followed with the exception of the C8 internal olefin concentration of the reaction fluid entering the vaporizer (15 wt. %).

5 Example 13. The procedure of Example 8 is followed with the exception of the C8 internal olefin concentration of the reaction fluid entering the vaporizer (20 wt. %).

10 Examples 8-13 model the effect of vaporizer condenser temperature and C8 internal olefin concentration of the reaction fluid entering the vaporizer on the average C8 internal olefin concentration in the reaction fluid within the strip gas vaporizer and in the vaporizer tails stream. Results for Examples 8-13 are shown in Table 3.

Table 3

	Strip gas condenser temp (°C)	C8 internal olefin concentration in the fluid entering the vaporizer (wt %)	Average C8 internal olefin concentration in the reaction fluid within the vaporizer (wt %)	C8 internal olefin concentration in the vaporizer tails (wt %)
Example 8	20	10	2.5	1.5
Example 9	30	10	3.1	1.8
Example 10	40	10	3.9	2.3
Example 11	50	10	5.1	3.0
Example 12	20	15	4.0	2.3
Example 13	20	20	5.7	3.2

15 The results of Examples 8-11 show that increasing the strip gas condenser temperature is an effective means of increasing the average C8 internal olefin concentration in the reaction fluid within the vaporizer and in the vaporizer tails stream. As shown in Examples 1-7, increasing the concentration of C8 internal olefins in the catalyst solution improves rhodium accountability in a high temperature, low CO partial pressure environment, such as exists in the vaporizer. Examples 12 and 13 illustrate the impact of increasing the C8 internal olefin concentration in the reaction fluid entering the vaporizer and in the vaporizer tails steam.

20

Example 14. The procedure of Example 8 is followed with the exception of the catalyst fluid being comprised of C8 internal olefin at 10 wt. %, C9 trimer at 45 wt. %, and nonanals (balance).

Example 15. The procedure of Example 8 is followed with the exception of the catalyst fluid being comprised of C8 internal olefin at 10 wt. %, C9 trimer at 20 %, and nonanals (balance).

5 Example 16. The procedure of Example 8 is followed with the exception of the catalyst fluid being comprised of C8 internal olefin at 10 wt. %, C9 trimer at 10 %, and nonanals (balance).

Examples 14-16 model the effect of C9 trimer (heavies) concentration on the average C8 internal olefin concentration in the reaction fluid within the strip gas vaporizer and in the vaporizer tails stream. Results for Examples 14-16 are shown in Table 4.

10

Table 4

	C9 trimer concentration in the fluid entering the vaporizer (wt %)	Average C8 internal olefin concentration in the reaction fluid within the vaporizer (wt %)	C8 internal olefin concentration in the vaporizer tails (wt %)
Example 14	45	2.3	1.2
Example 15	20	3.4	2.1
Example 16	10	3.5	2.2

15

The results of Table 4 show that, at a constant feed to tails ratio, lowering the heavies concentration in the reaction fluid (e.g., through taking a purge of the vaporizer tails) will increase the average C8 internal olefin concentration in the reaction fluid within the vaporizer and in the vaporizer tails stream.

Comparative Experiment C. The procedure of Example 8 is followed with the exception of the target feed to tails ratio being 3 : 1.

Comparative Experiment D. The procedure of Example 8 is followed with the exception of the target feed to tails ratio being 2.5 : 1.

20

Example 17. The procedure of Example 8 is followed with the exception of the target feed to tails ratio being 1.5 : 1.

25

Comparative Experiments C-D and Example 7 model the effect of feed to tails ratio for the strip gas vaporizer (the ratio of the mass of reaction fluid fed to the strip gas vaporizer to the mass of the vaporizer tails stream) on the average C8 internal olefin concentration in the reaction fluid within the strip gas vaporizer and in the vaporizer tails. The results of Comparative Experiments C, D and Example 17 are summarized in Table 5.

Table 5

	Target feed to tails ratio	Average C8 internal olefin concentration in the reaction fluid within the vaporizer (wt %)	C8 internal olefin concentration in the vaporizer tails (wt %)
Comparative Experiment C	3 : 1	1.3	0.7
Comparative Experiment D	2.5 : 1	1.9	1.0
Example 17	1.5 : 1	3.7	2.4

The results of Table 5 show that lowering the feed to tails ratio will increase the average C8 internal olefin concentration in the vaporizer and in the vaporizer tails stream, and thereby improve rhodium accountability.

Example 18-47 and Comparative Experiments E-G (C. E. E – C. E. G). The model described in Example 8 is used to calculate the average concentration of C8 internal olefins in the reaction fluid within the vaporizer and the concentration of C8 internal olefins in the vaporizer tails over a range of conditions. In each case the parameters are established as indicated in Table 6, and the strip gas flow is varied in order to achieve the target feed to tails ratio.

Table 6

	Vaporizer Conditions			Composition of Reaction fluid entering the vaporizer (wt%)				Strip gas details		Concentration of C8 internal olefins (wt%)	
	Vap Temp (°C)	Vap Press (PSIA)	F:T	internal C8 olefin	C9 trimer	1-nonanal	isononanal	C8 internal olefins in strip gas (wt%)	condenser temp (°C)	in the fluid within the vaporizer (average)	in vaporizer tails
Example 18	100	22	2	10.00	30.00	3.00	57.00	1.61	20	2.52	1.46
Example 19	100	22	2	10.00	30.00	3.00	57.00	2.67	30	3.09	1.80
Example 20	100	22	2	10.00	30.00	3.00	57.00	4.19	40	3.93	2.31
Example 21	100	22	2	10.00	30.00	3.00	57.00	6.21	50	5.06	3.01
C.E.E.	100	22	2	5.00	30.00	3.25	61.75	0.93	20	1.23	0.73
Example 22	100	22	2	10.00	30.00	3.00	57.00	1.61	20	2.52	1.46
Example 23	100	22	2	15.00	30.00	2.75	52.25	2.12	20	3.97	2.25
Example 24	100	22	2	20.00	30.00	2.50	47.50	2.51	20	5.69	3.15
Example 25	100	22	2	10.00	45.00	2.25	42.75	2.73	30	2.26	1.23
Example 26	100	22	2	10.00	30.00	3.00	57.00	2.67	30	3.10	1.81
Example 27	100	22	2	10.00	20.00	3.50	66.50	2.64	30	3.35	2.06
Example 28	100	22	2	10.00	10.00	4.00	76.00	2.61	30	3.52	2.23
Example 29	100	22	1.5	10.00	30.00	3.00	57.00	2.00	20	3.74	2.38
Example 30	100	22	2	10.00	30.00	3.00	57.00	1.61	20	2.52	1.46
C.E.F.	100	22	2.5	10.00	30.00	3.00	57.00	1.45	20	1.91	1.02
C.E.G.	100	22	3	10.00	30.00	3.00	57.00	1.35	20	1.30	0.68
Example 31	80	22	2	10.00	30.00	3.00	57.00	1.60	20	2.38	1.74
Example 32	85	22	2	10.00	30.00	3.00	57.00	1.61	20	2.39	1.63
Example 33	90	22	2	10.00	30.00	3.00	57.00	1.61	20	2.42	1.55
Example 34	95	22	2	10.00	30.00	3.00	57.00	1.62	20	2.47	1.50
Example 35	100	22	2	10.00	30.00	3.00	57.00	1.61	20	2.52	1.46
Example 36	105	22	2	10.00	30.00	3.00	57.00	1.61	20	2.59	1.45
Example 37	110	22	2	10.00	30.00	3.00	57.00	1.61	20	2.68	1.44
Example 38	80	22	2	10.00	30.00	3.00	57.00	4.01	40	4.46	3.33
Example 39	85	22	2	10.00	30.00	3.00	57.00	4.06	40	4.29	2.98
Example 40	90	22	2	10.00	30.00	3.00	57.00	4.11	40	4.15	2.70
Example 41	95	22	2	10.00	30.00	3.00	57.00	4.15	40	4.02	2.48
Example 42	100	22	2	10.00	30.00	3.00	57.00	4.18	40	3.92	2.30
Example 43	105	22	2	10.00	30.00	3.00	57.00	4.20	40	3.84	2.17
Example 44	110	22	2	10.00	30.00	3.00	57.00	4.22	40	3.79	2.06
Example 45	100	8	2	10.00	30.00	3.00	57.00	4.30	20	2.59	1.44
Example 46	100	15	2	10.00	30.00	3.00	57.00	2.34	20	2.55	1.45
Example 47	100	22	2	10.00	30.00	3.00	57.00	1.61	20	2.52	1.46

The calculated average concentration of C8 internal olefins in the fluid within the vaporizer is plotted versus the concentration of internal C8 olefins in the vaporizer tails stream for each case shown in Table 6, and the result is shown in Figure 1.

Examples 1-7 demonstrate that a C8 internal olefin concentration of > 2 wt % in the fluid within the vaporizer will improve rhodium accountability. The plot of Figure 1 shows that when the C8 internal olefins concentration in the vaporizer tails stream is at least 1.2 wt %, the average concentration of C8 internal olefins in the fluid within the vaporizer is calculated to be greater than 2 wt %. A similar process can be used to determine the average concentration of C9 internal olefins in the fluid within the vaporizer or a simple molar scaling factor can be used based on the molecular weight of the olefin compared to

mixed octenes to keep the molar concentration of olefin above the equivalent of 1.2 wt% C8 internal olefins.

Thus monitoring the concentration of C8 internal olefins in the vaporizer tails stream, and taking one or more actions to achieve or maintain that concentration at ≥ 1.2 wt %
5 %, will achieve the result of the invention, specifically improving the rhodium accountability in a hydroformylation process comprising rhodium, an organomonophosphite ligand and mixed C8 olefins.

WHAT IS CLAIMED IS:

1. A process to improve rhodium accountability in a continuous liquid recycle hydroformylation process, the process comprising:
 - contacting in a reaction zone reactants comprising mixed C8 olefins and/or mixed C9 olefins, hydrogen, and carbon monoxide in the presence of a catalyst comprising rhodium and an organomonophosphate ligand to form a reaction fluid, wherein the reaction fluid is introduced to a strip gas vaporizer to produce a product stream and a vaporizer tails stream, and wherein the vaporizer tails stream comprises at least 1.2 percent by weight C8 internal olefins or at least 1.3 percent by weight C9 internal olefins.
2. The process of claim 1, further comprising increasing the C8 internal olefin concentration or the C9 internal olefin concentration in the vaporizer tails stream by one or more of:
 - (a) increasing the C8 internal olefin concentration or the C9 internal olefin concentration in the reaction fluid entering the strip gas vaporizer; or
 - (b) lowering the heavies concentration in the reaction fluid entering the strip gas vaporizer; or
 - (c) lowering the ratio of the mass of reaction fluid fed to the strip gas vaporizer to the mass of the vaporizer tails stream; or
 - (d) raising the temperature of a strip gas condenser associated with the strip gas vaporizer.
3. The process of claim 1 or claim 2, further comprising removing olefins from the product stream and returning the removed olefins to the reaction zone.
4. The process of claim 2, wherein the C8 olefin concentration or the C9 internal olefin concentration in the vaporizer tails stream is increased by increasing the C8 olefin concentration or the C9 internal olefin concentration in the reaction fluid entering the strip gas vaporizer, wherein the C8 internal olefin concentration or the C9 internal olefin concentration in the reaction fluid entering the strip gas vaporizer is increased by decreasing the hydroformylation rate in the reaction zone or by reducing the rate of olefin conversion in

the reaction zone.

5. The process of claim 4, wherein the C8 internal olefin concentration or the C9 internal olefin concentration in the vaporizer tails stream is increased by reducing the rate of olefin conversion in the reaction zone, wherein the rate of olefin conversion in the reaction zone is reduced by (a) lowering the residence time of the reaction fluid within the reaction zone, (b) increasing the mixed C8 olefin feed rate or the C9 olefin feed rate, (c) increasing the feed of recycled olefins to the reaction zone, (d) increasing the proportion of recycled olefin being fed to the reaction zone, or a combination thereof.

6. The process of claim 2, wherein the process comprises lowering the ratio of the mass of reaction fluid fed to the strip gas vaporizer to the mass of the vaporizer tails stream and wherein the ratio is greater than 1 to 3.

7. The process of claim 1 or claim 2, further comprising removing olefins from the product stream and returning the removed olefins to the reaction fluid before introduction into the strip gas vaporizer.

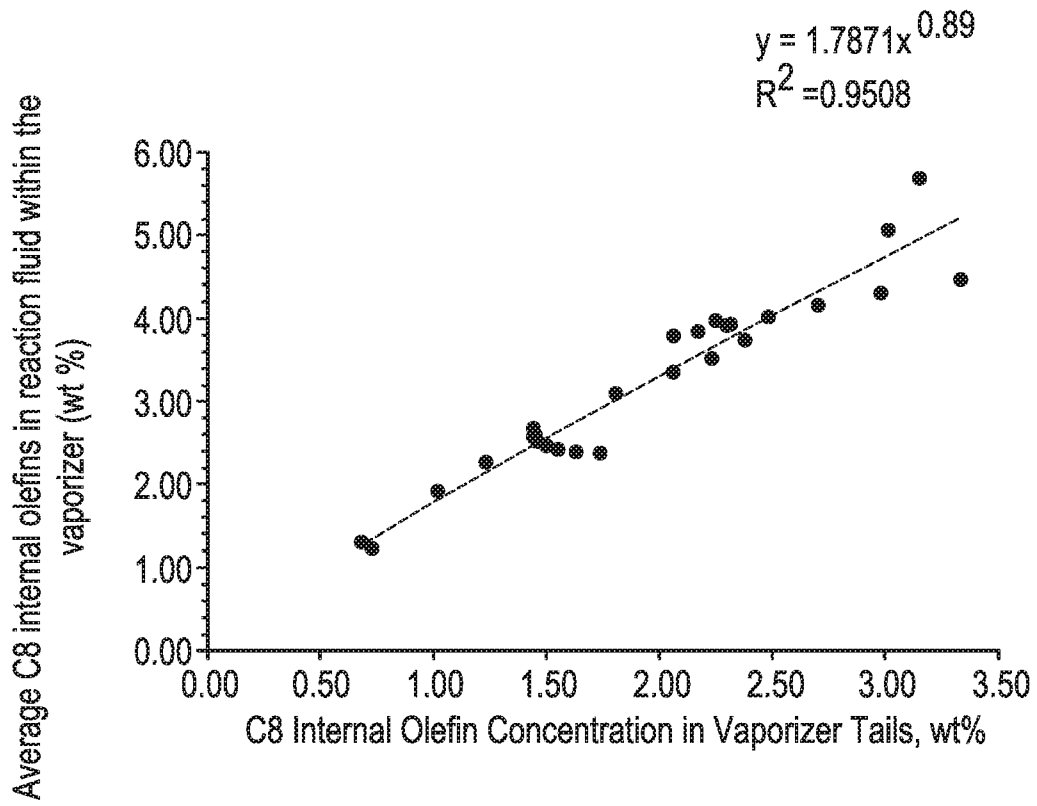
8. The process of claim 2 comprising increasing the C8 internal olefin concentration in the vaporizer tails stream by two or more of:

- (a) increasing the C8 internal olefin concentration in the reaction fluid entering the strip gas vaporizer; or
- (b) lowering the heavies concentration in the reaction fluid entering the strip gas vaporizer; or
- (c) lowering the ratio of the mass of reaction fluid fed to the strip gas vaporizer to the mass of the vaporizer tails stream ; or
- (d) raising the temperature of a strip gas condenser associated with the strip gas vaporizer.

9. The process of any of the preceding claims, wherein the vaporizer tails stream comprises at least 1.4 percent by weight C8 internal olefins.

10. The process of claim 9, wherein the vaporizer tails stream comprises 1.4 to 15 percent by weight C8 internal olefins.

FIG. 1



INTERNATIONAL SEARCH REPORT

International application No
PCT/US2019/061509

A. CLASSIFICATION OF SUBJECT MATTER
INV. C07C45/50 C07C47/02
ADD.
According to International Patent Classification (IPC) or to both national classification and IPC

B. FIELDS SEARCHED
Minimum documentation searched (classification system followed by classification symbols)
C07C
Documentation searched other than minimum documentation to the extent that such documents are included in the fields searched

Electronic data base consulted during the international search (name of data base and, where practicable, search terms used)
EPO-Internal, WPI Data

C. DOCUMENTS CONSIDERED TO BE RELEVANT

Category*	Citation of document, with indication, where appropriate, of the relevant passages	Relevant to claim No.
A	WO 2016/089602 A1 (DOW TECHNOLOGY INVESTMENTS LLC [US]) 9 June 2016 (2016-06-09) examples 12-17 figure 1	1-10
A	US 4 443 638 A (YATES JAMES A [US]) 17 April 1984 (1984-04-17) column 1, line 46 - column 3, line 8 column 4, line 10 - line 35 example 2	1-10

Further documents are listed in the continuation of Box C.

See patent family annex.

* Special categories of cited documents :

"A" document defining the general state of the art which is not considered to be of particular relevance

"E" earlier application or patent but published on or after the international filing date

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"O" document referring to an oral disclosure, use, exhibition or other means

"P" document published prior to the international filing date but later than the priority date claimed

"T" later document published after the international filing date or priority date and not in conflict with the application but cited to understand the principle or theory underlying the invention

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"Y" document of particular relevance; the claimed invention cannot be considered to involve an inventive step when the document is combined with one or more other such documents, such combination being obvious to a person skilled in the art

"&" document member of the same patent family

Date of the actual completion of the international search 26 February 2020	Date of mailing of the international search report 12/03/2020
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Name and mailing address of the ISA/ European Patent Office, P.B. 5818 Patentlaan 2 NL - 2280 HV Rijswijk Tel. (+31-70) 340-2040, Fax: (+31-70) 340-3016	Authorized officer Patteux, Claudine
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INTERNATIONAL SEARCH REPORT

International application No
PCT/US2019/061509

C(Continuation). DOCUMENTS CONSIDERED TO BE RELEVANT		
Category*	Citation of document, with indication, where appropriate, of the relevant passages	Relevant to claim No.
A	JÖRKE ANDREAS ET AL: "Hydroformylation and tandem isomerization-hydroformylation of n-decenes using a rhodium-BiPhePhos catalyst: Kinetic modeling, reaction network analysis and optimal reaction control", CHEMICAL ENGINEERING JOURNAL, ELSEVIER, AMSTERDAM, NL, vol. 313, 20 December 2016 (2016-12-20), pages 382-397, XP029900714, ISSN: 1385-8947, DOI: 10.1016/J.CEJ.2016.12.070 paragraph [05.3]	1-10
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INTERNATIONAL SEARCH REPORT

Information on patent family members

International application No

PCT/US2019/061509

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